

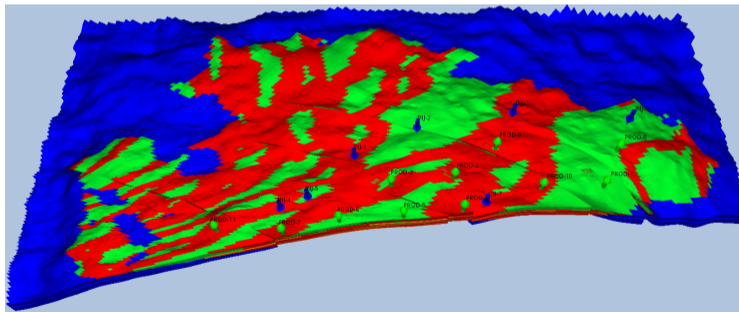
# Olympus Optimization under Geological Uncertainty

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- ▶ Task 1: Well Control Optimization
- ▶ Task 2: Field Development Optimization
- ▶ Task 3: Joint Field Development and Well Control Optimization



- ▶ Objective function:

$$NPV = \sum_{i=1}^{N_t} \frac{R(t_i)}{(1 + d)^{t_i/\tau}},$$

- ▶ Revenue term:

$$R(t_i) = Q_{op}(t_i) \cdot r_{op} - Q_{wp}(t_i) \cdot r_{wp} - Q_{wi}(t_i) \cdot r_{wi} - P(t_i) - D(t_i).$$

$P(t_i)$  - platform cost,  $D(t_i)$  - drilling cost.

- ▶ Pre-conditioned steepest ascend:

$$x_{k+1} = x_k + \eta_k C \nabla J_k$$

- ▶ Gradient approximation with geological uncertainty:

$$\nabla J_k \approx N^{-1} \sum_{i=1}^N [J(x_k^i, y^i) - J(x_k, y^i)] [x_k^i - x_k]$$

- ▶ For more information we refer to:

Fonseca et al. (2017), Stordal et al. (2016), Chen et al. (2009), Lorentzen et al. (2006)

- ▶ Based on evaluation of simplex points (Hooke-Jeeves):

$$J(x_k + \alpha e_j) = J(z_j), \quad j = 1, \dots, N_x, \quad x_k \leftrightarrow z_{\text{best}}$$

- ▶ Method enhanced using line search:

$$x_{k+1} = x_k + \eta_k G_k$$

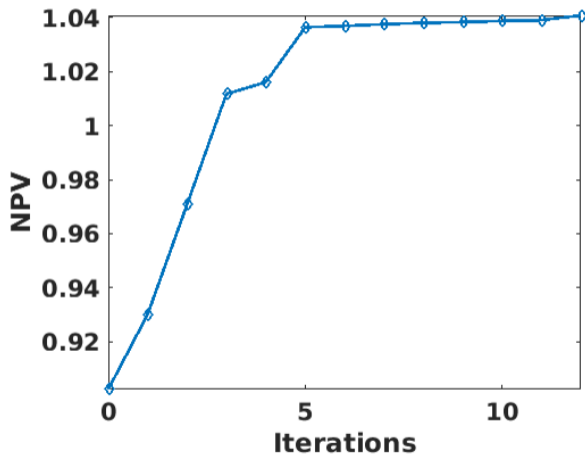
- ▶ A simplex gradient is computed as:

$$G_k = [z_1 - x_k, \dots, z_{N_x} - x_k]^{-1} [J(z_1) - J(x_k), \dots, J(z_{N_x}) - J(x_k)]^T$$

- ▶ For more information we refer to:  
Asadollahi et al. (2014)

- ▶ EnOpt with backtracking is applied,  $N = 50$ ,  $\eta_k = 0.5$
- ▶ Control variables are shut-in times for producers, and pressures for injectors
- ▶ Initial mean for parameters obtained using the TNO reference case
- ▶ Ensemble generated by drawing perturbations  $\sim \mathcal{N}(0, 0.01)$

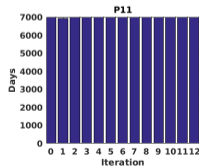
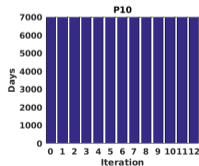
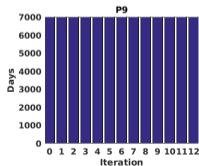
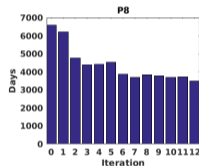
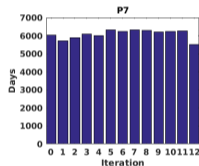
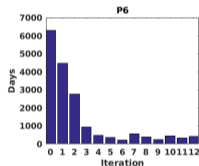
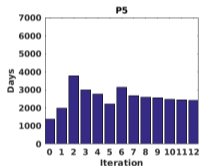
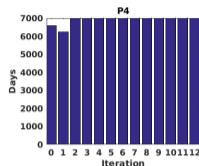
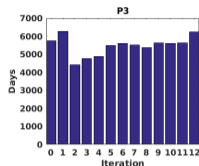
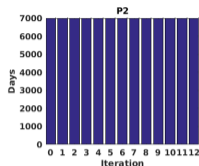
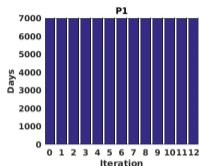
# Task 1: Scaled NPV as function of iterations



$$NPV_{\text{ref}} = \$1.4875 \cdot 10^9$$

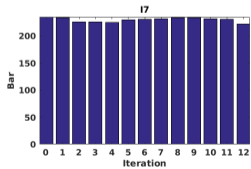
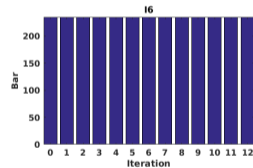
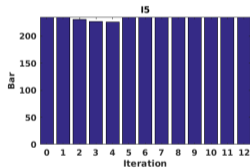
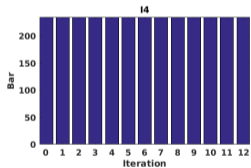
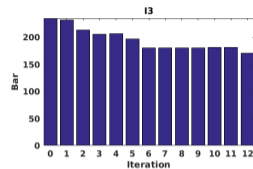
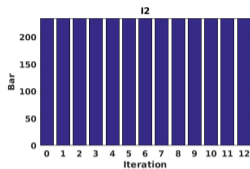
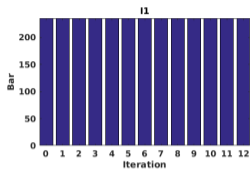
$$NPV_{\text{max}} = \$1.5480 \cdot 10^9$$

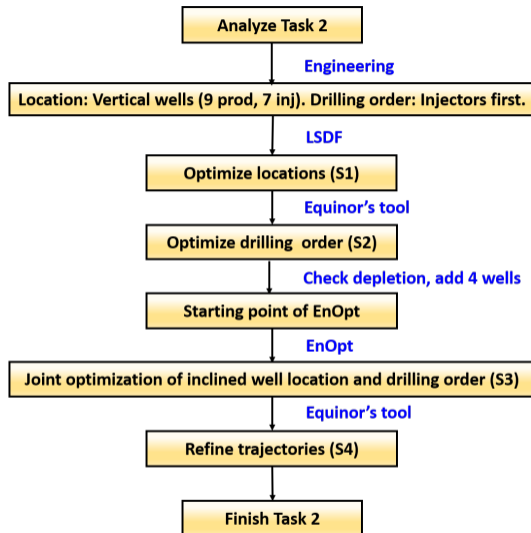
# Task 1: Shut-in times as function of iterations



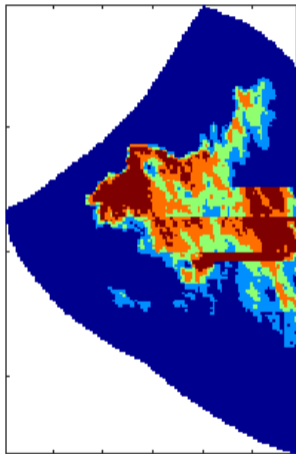


# Task 1: Injection pressures as function of iterations

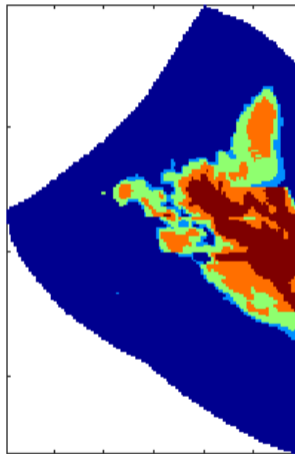




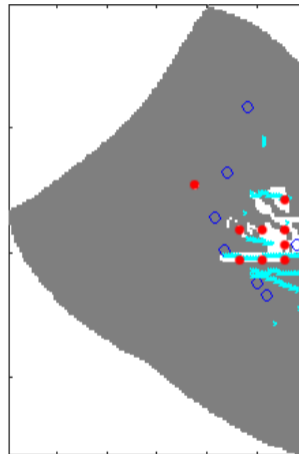
## Task 2: Engineering judgment



OIP top zone

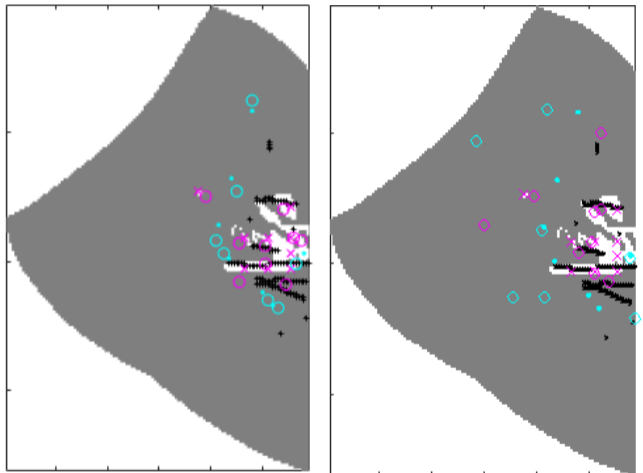


OIP bottom zone



Target map

## Task 2: Vertical well optimization (S1)



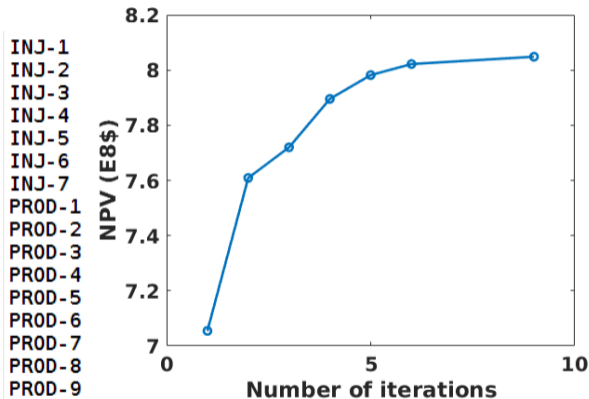
$$\begin{aligned} \text{NPV}_{\text{ref}} &= \$0.35 \cdot 10^9 \\ \text{NPV}_{\text{S1}} &= \$0.70 \cdot 10^9 \end{aligned}$$

Legend:

- × : initial producers
- : final producers
- × : initial injectors
- : final injectors
- : reference producers

EnOpt (left) and LSDF (right) on vertical well optimization (S1)

## Task 2: Drilling order optimization (S2)



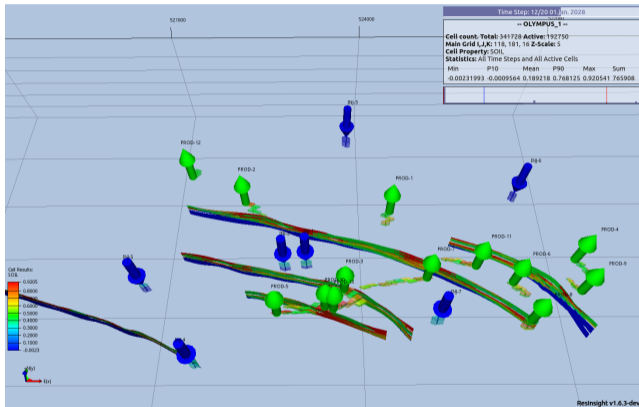
PROD-3	$NPV_{ref} = \$0.35 \cdot 10^9$
INJ-5	$NPV_{S1} = \$0.70 \cdot 10^9$
PROD-7	$NPV_{S2} = \$0.81 \cdot 10^9$
PROD-5	
INJ-6	
INJ-2	

Equinor's internal tool

For more information:  
Hanea et al. (2016)

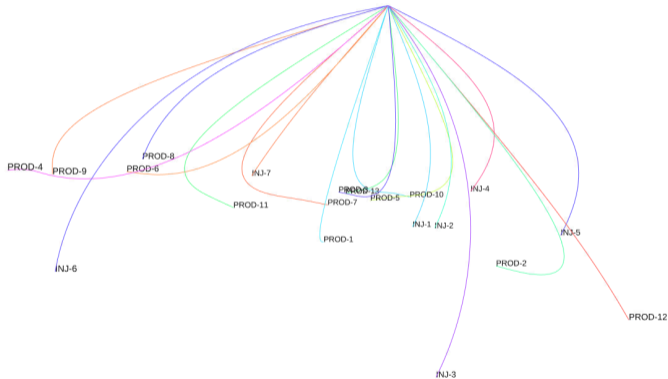
PROD-1  
PROD-4  
INJ-7  
PROD-6  
PROD-9  
PROD-2  
INJ-1  
INJ-3  
INJ-4  
PROD-8

# Task 2: EnOpt on inclined well optimization (S3)



- PROD-3
  - PROD-7
  - INJ-1
  - PROD-1
  - INJ-5
  - PROD-5
  - INJ-7
  - PROD-11
  - INJ-2
  - INJ-6
  - PROD-4
  - PROD-2
  - INJ-3
  - PROD-10
  - PROD-8
  - PROD-12
  - INJ-4
  - PROD-9
  - PROD-6
  - PROD-13
- $NPV_{ref} = \$0.35 \cdot 10^9$   
 $NPV_{S1} = \$0.70 \cdot 10^9$   
 $NPV_{S2} = \$0.81 \cdot 10^9$   
 $NPV_{S3} = \$0.94 \cdot 10^9$
- $U_{prod} = \begin{bmatrix} x_{hp} \\ y_{hp} \\ x_{tp} \\ y_{tp} \\ z_{tp} \end{bmatrix}, U_{inj} = \begin{bmatrix} x_{hi} \\ y_{hi} \\ z_{ti} \end{bmatrix}$

## Task 2: Final results (S4)



$$\begin{aligned} NPV_{\text{ref}} &= \$0.35 \cdot 10^9 \\ NPV_{S1} &= \$0.70 \cdot 10^9 \\ NPV_{S2} &= \$0.81 \cdot 10^9 \\ NPV_{S3} &= \$0.94 \cdot 10^9 \\ NPV_{S4} &= \$1.15 \cdot 10^9 \end{aligned}$$

Equinor's internal tool,  
combining EnOpt and RMS

For more information:  
Hanea et al. (2017)

- ▶ Final well trajectories from Task 2 (S4) is used
- ▶ LSDF is run using three geomodels
- ▶ Control variables are shut-in times for producers, and pressures for injectors
- ▶ Initial mean for parameters obtained using the TNO reference case
- ▶ Final  $NPV_{\max} = \$1.15 \cdot 10^9$

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	P1	P2	P3	P4	P5	P6	P7	P8	P9	P10	P11	P12	P13
Initial	20.0	20.0	20.0	13.2	20.0	20.0	20.0	20.0	20.0	20.0	20.0	17.7	20.0
Optimal	20.0	20.0	9.74	11.4	20.0	20.0	14.5	13.6	15.4	20.0	20.0	11.6	13.3

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	<b>Task 1</b>	<b>Task 2</b>	<b>Task 3</b>
$NPV_{\text{ref}} (10^9 \$)$	1.49	0.35	1.15
$NPV_{\text{ini}} (10^9 \$)$	1.34	0.35	1.01
$NPV_{\text{max}} (10^9 \$)$	1.55	1.147	1.153
$P_{\text{ref}} (\%)$	4.1	230	0.52
$P_{\text{ini}} (\%)$	16	230	14
$N_{\text{sim}}$	1450	1750	1209
$N_{\text{core}}$	25	25/3	3

## We thank

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- ▶ Schlumberger for providing academic software licenses to ECLIPSE.
- ▶ The authors acknowledge the Research Council of Norway and the industry partners, ConocoPhillips Skandinavia AS, Aker BP ASA, Vår Energi AS, Equinor ASA, Neptune Energy Norge AS, Lundin Norway AS, Halliburton AS, Schlumberger Norge AS, Wintershall Norge AS, and DEA Norge AS, of The National IOR Centre of Norway for support.

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